DICP Course - Dalian, 2012 Preparation of solid catalysts Part 1

Supported by the Chinese Academy of Sciences

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DALIAN INSTITUTE OF CHEMICAL PHYSICS, CHINESE ACADEMY OF SCIENCES







Preparation of catalysts 1

Introduction and general aspects

Interfacial chemistry – Electrostatic adsorption

Impregnation and drying

Sol-gel chemistry processing

Deposition – Precipitation – Coprecipitation

Shaping of solid catalysts – Monolith-based catalysts

Zeolite-based catalysts

<u>Characterization – High throughput experimentation</u>

Case studies:

- Noble metal catalysts
- Methanol catalysts
- Hydrotreating catalysts
-

Introduction and general aspects

1) Importance and development of solid catalysts

2) What is catalysis ?

A short introduction

Surface reactions, physisorption, chemisorption Kinetics and catalysis

3) What is a solid catalyst ?

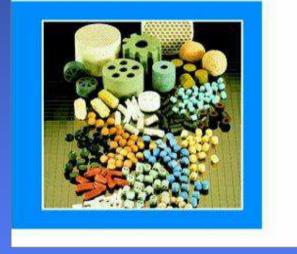
Preparation : carrier, precursor, active phase Characterization : surface area, metallic area, size, porosity Active centers : stability, activity, selectivity

Importance and development of solid catalysts: some books

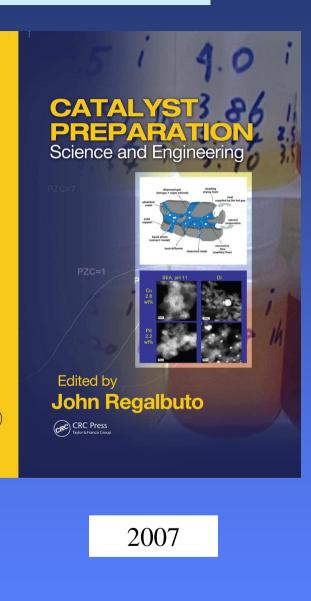
WILEY-VCH

Preparation of Solid Catalysts

Edited by G. Ertl, H. Knözinger, J. Weitkamp



1999



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Importance and development of solid catalysts: some books



WILEY-VCH

Importance and development of solid catalysts

•About 85 % of all chemical processes make use of catalysts

•All molecules of modern fuels have been confronted at least with one catalyst

World catalyst demand and forecast (billion US \$/year) by application [de Jong, 2009]

		2007	2010	2013	
	Refining	4.35	4.98	5.85	
	Petrochemicals	3.03	3.64	4.34	
	Polymers	3.24	3.75	4.30	
	Fine chemicals/other	1.47	1.59	1.70	
	Environmental	5.51	6.28	6.93	
	Total	17.6	20.2	23.1	
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Importance and development of solid catalysts

Chemical C_2H_4, C_3H_6 H_2SO_4 Ammonia Nitric acid Saturated chemicals Polymers Epoxide Methanol Fuel, gazoline Gazoline Gazoline Gazoline Clean air

Application reaction

hydrocarbon cracking $SO_2 + 0.5 O_2 \rightarrow SO_3 \rightarrow H_2SO_4$ $N_2 + H_2 \rightarrow NH_3$ $NH_3 + O_2 \rightarrow NO_2 \rightarrow HNO_3$ hydrogenation polymerization $C_2H_4 + O_2 \rightarrow C_2H_4O$ $CO + 2 H_2 \rightarrow CH_3OH$ hydrotreating **Fischer-Tropsch** synthesis hydroisomerization catalytic cracking NO_x abatement

Catalyst Pt/SiO₂-Al₂O₃ V_2O_5 K₂O/Fe/Al₂O₃ Pt-Rh Ni/SiO₂ CrO_x/SiO_2 $Ag/\alpha - Al_2O_3$ Cu/ZnO/Al₂O₃ $CoMoS_{2}/\gamma - Al_{2}O_{3}$ Co/SiO₂ Pt/mordenite Zeolite Y based V_2O_5/TiO_2

The Past

- Use of catalytic reactions since ancient time but not recognized due to the lack of scientific knowledge. Ex.: fermentation to produce ethanol.
 - $C_6H_{12}O_6(aq) \rightarrow 2 C_2H_5OH(l) + 2 CO_2(g)$
- Use of sulfuric acid to catalyze the synthesis of diethylether (16th century).
 - $2 C_2 H_5 OH(1) \rightarrow C_2 H_5 O-C_2 H_5(1) + H_2 O(1)$
- Production of sulfuric acid using nitrogen oxides (18th century).

19th century. Discoveries in chemical reaction rates (<u>Humphry Davy, Michael Faraday</u>)

The Davy lamp: can burn methane without flame

 $CH_4 + 2 O_2 \rightarrow CO_2 + 2 H_2O$

use of platinum gauze to control this reaction without flame propagation

➔ First use for human safety: the presence of methane pockets in mines could be detected before the explosion happens.

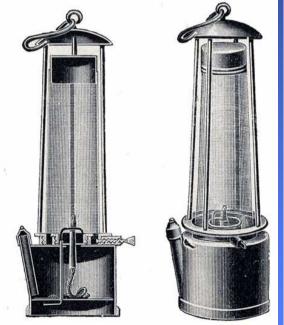


Fig. 192. Davniche Sicherheitslampe

J. Berzelius introduce the word "catalysis" in 1836. Catalysis derived from Greek roots: *cata* = down, *lysein* = split or break Example: decomposition of H_2O_2 :

 $H_2O_2(l) \rightarrow H_2O(l) + 1/2 O_2(g)$

"Catalytic power actually means that substances are able to awaken affinities which are asleep at this temperature by their mere presence and not by their own affinity."

Usually accepted definition :

A <u>catalyst</u> is a substance that increases the <u>rate</u> at which a chemical system approaches <u>equilibrium</u>, without being consumed in the process.

<u>Catalysis</u> is the phenomenon of a catalyst in action.

The original text (translated in English)

"This is a new power to produce <u>chemical activity</u> belonging to both inorganic and organic nature, which is surely more widespread than we have hitherto believed and the nature of which is still concealed from us. When I call it a new power, I do not mean to imply that it is a capacity independent of the <u>electrochemical properties</u> of the substance. On the contrary, I am unable to suppose that this is anything other than a kind of special manifestation of these, but as long as we are unable to discover their mutual relationship, it will simplify our researches to regard it as a separate power for the time being. It will also make it easier for us to refer to it if it possesses a name of its own.

I shall therefore using a derivation well-known in chemistry, call it the <u>catalytic power of</u> <u>the substances</u>, and the decomposition by means of this power <u>catalysis</u>, just as we use the word analysis to denote the separation of the component parts of bodies by means of ordinary chemical forces. <u>Catalytic power</u> actually means that substances are able to awaken affinities which are asleep at this temperature by their mere presence and not by their own affinity.

Heterogeneous catalysis (80 wt.-%)

The reactants and the catalyst are present in different phases:

 \rightarrow reactants: gas or liquid phase

→ catalyst: solid phase

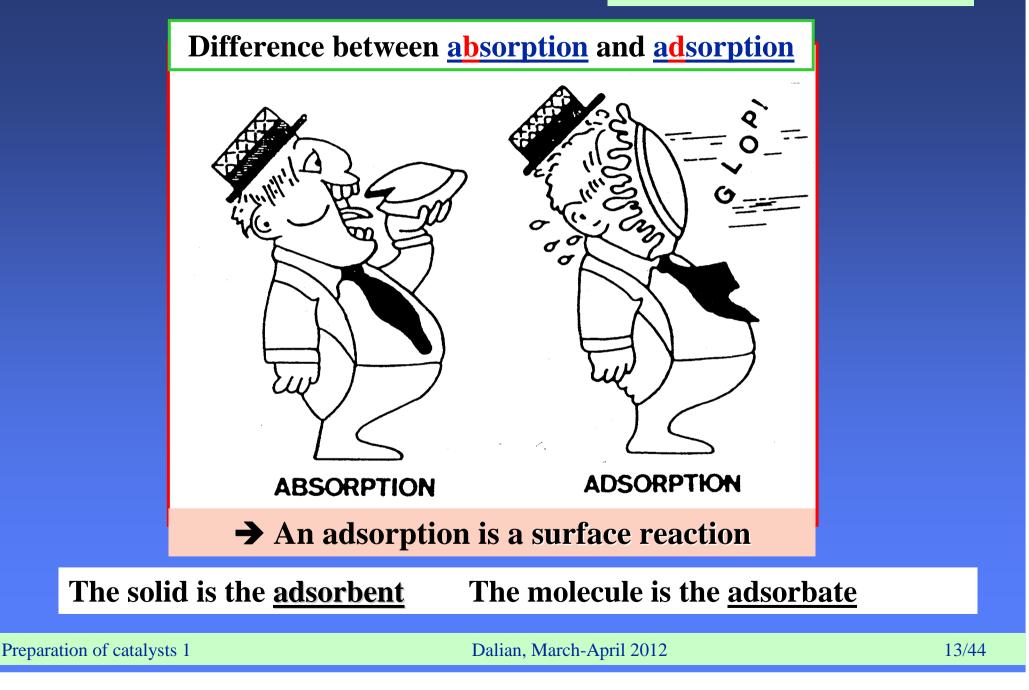
The catalytic reactions happen at the surface of the solid.

Homogeneous catalysis (17 %) and biocatalysis (3 %)

The reactants and the catalyst are present in the same phase : liquid phase.

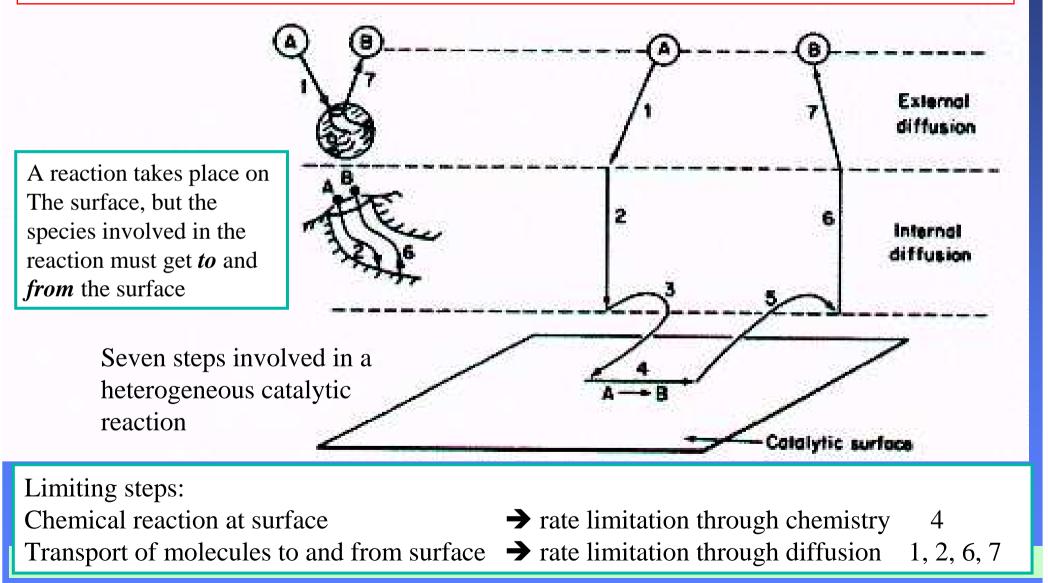
The catalyst is a solute of the system.

Surface reactions



Mechanism of catalytic reactions

The essence of catalysis is a <u>cycle</u> of reactions that consumes the reactants, forms the products and regenerates the catalytic species for a new cycle [Bond, 1987].



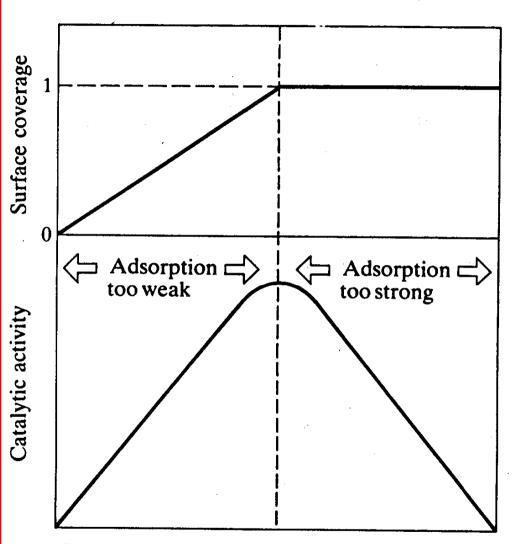
Volcano plot

Which metal is the best catalyst for a given reaction ?

The catalytic activity is inversely related to the strength of chemisorption of the reactants providing that adsorption is sufficiently strong for the adsorbate to achieve high surface coverage. (Balandine, 1925)

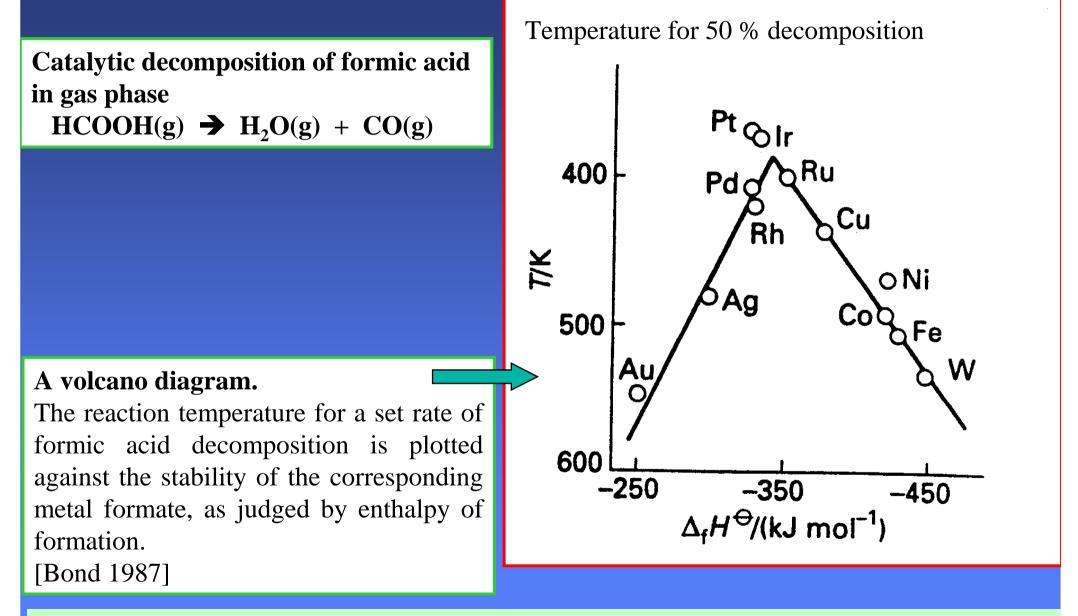
The volcano curve:

dependence of catalytic activity upon strength of reactant adsorption (lower part) and the corresponding variation in surface coverage (upper part).



Parameter measuring strength of adsorption

An example of volcano plot



Session I – Catalysis and Catalysts

1) What is catalysis ?

A short introduction

Surface reactions, physisorption, chemisorption

Kinetics and catalysis

2) What is a solid catalyst ?

Preparation : carrier, precursor, active phase Characterization : surface area, metallic area, size, porosity Active centers : stability, activity, selectivity

- High surface area
- Low pressure drop
- High number of active sites

Classification of heterogeneous catalysts

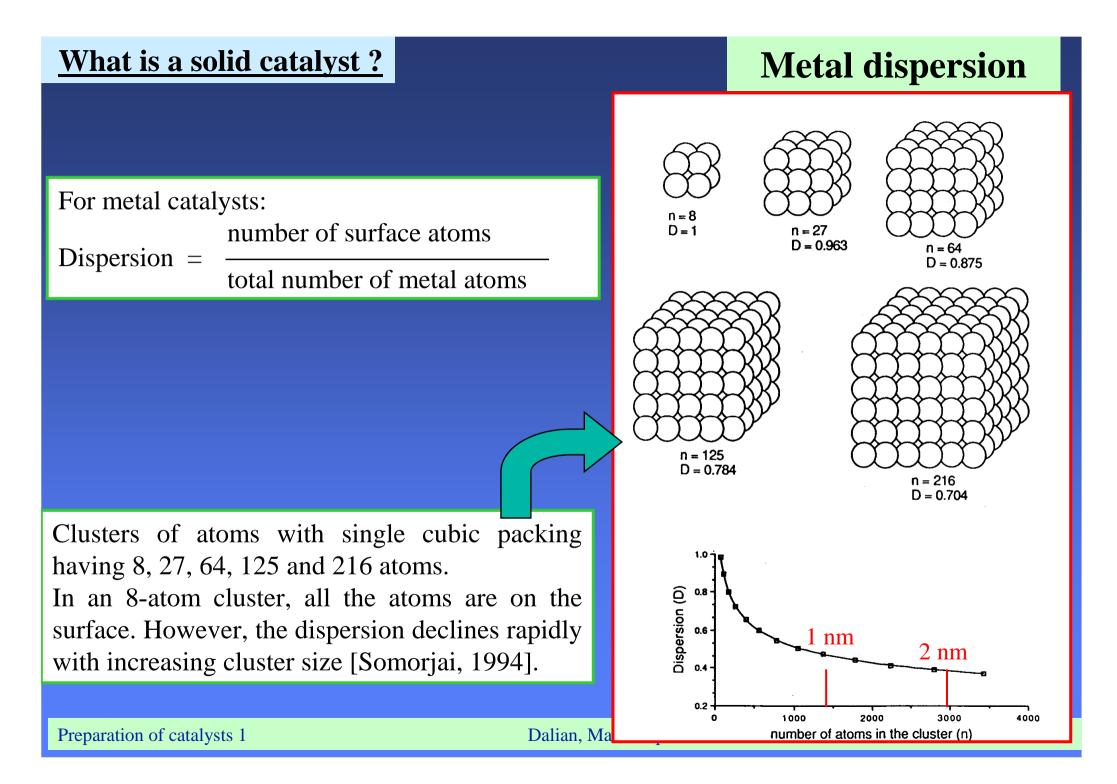
Class	Functions	Examples
Metals, alloys conductors	hydrogenation dehydrogenation hydrogenolysis	Fe, Ni, Pd, Pt, Ag
Oxides and sulphides block d Semiconductors	oxidation dehydrogenation desulphurization	NiO, ZnO, MnO2 Cr ₂ O ₃ , Bi ₂ O ₃ -MoO ₃ WS ₂
Insulator oxides blocks s and p	dehydration	Al ₂ O ₃ , SiO ₂ , MgO
Acids, zeolites	polymerization isomerization cracking, alkylation	$H_{3}PO_{4}, H_{2}SO_{4}$ $SiO_{2}-Al_{2}O_{3}$
	isomerization	<i>v</i> . –

The periodic table

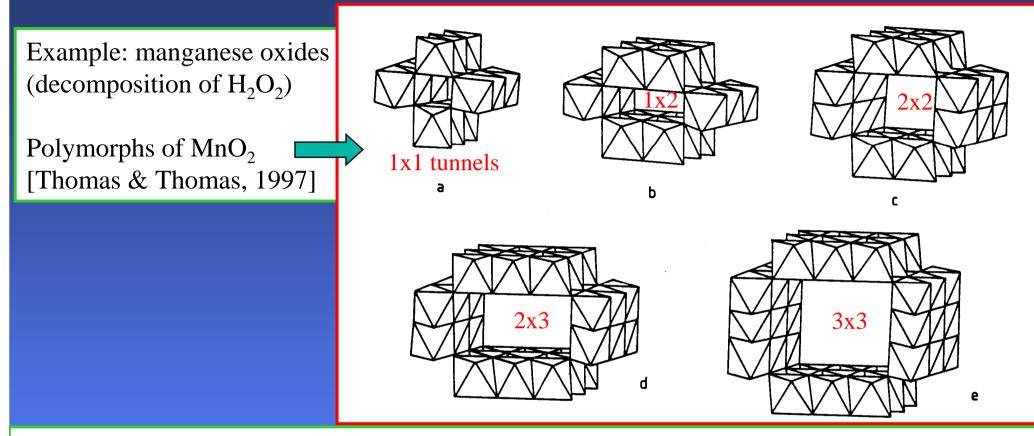
What is a solid catalyst ?

																	18
1	2							Η				13	14	15	16	17	He
Li	Be											В	С	Ν	0	F	Ne
Na	Mg	3	4	5	6	7	8	9	10	11	12	<mark>Al</mark>	<mark>Si</mark>	Р	S	Cl	Ar
K	Ca	Sc	Ti	V	Cr	Mn	Fe	Co	<mark>Ni</mark>	Cu	Zn	Ga	Ge	As	Se	Br	Kr
Rb	Sr	Y	Zr	Nb	Mo	Tc	Ru	<mark>Rh</mark>	<mark>Pd</mark>	Ag	Cd	In	Sn	Sb	Te	Ι	Xe
Cs	Ba	Lu	Hf	Та	W	Re	Os	<mark>Ir</mark>	<mark>Pt</mark>	Au	Hg	Tl	Pb	Bi	Po	At	Rn
Fr	Ra	Lr															
s bl	oolz					dh	lock							n h	lock		
5 01	UCK					u D.	IUCK							h n	IUCK		
la	antha	nides	s	La	Ce	Pr	Nd	Pm	Sm	Eu	Gd	Tb	Dy	Но	Er	Tm	Yb
actinides Ac Th Pa U			U	Np	Pu	Am	Cm	Bk	Cf	Es	Fm	Md	No				
	f block																

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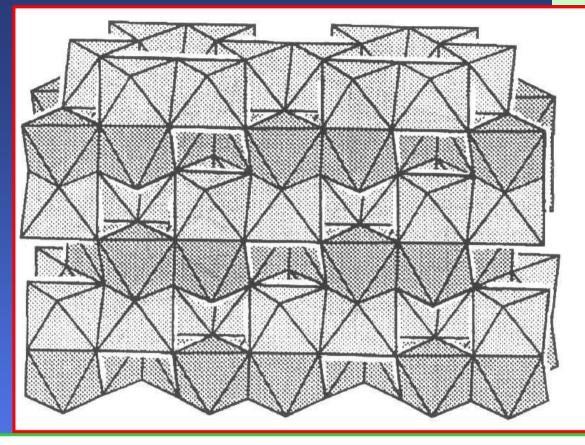
Semiconducting oxides



- (a) Pyrolusite β -MnO₂ has the rutile structure;
- (b) ramsdellite γ -MnO₂ has the structure of the mineral diaspore;
- (c) hollandite α -MnO₂ has tunnels circumscribed by a 2 x 2 arrangement of edge-sharing octahedra;
- (d) romanechite displays 2 x 3 tunnels;
- (e) todorkite displays 3 x 3 tunnels.

→ What is the best structure for the decomposition of hydrogen peroxide?

Insulator oxides



Alumina

Linked octahedra in corundum α -Al₂O₃. The Al atoms are at the centers and the O atoms at the corners of the octahedra. (U. Müller, Inorganic structural chemistry, Wiley, 1992, p. 171).

- **→** Low specific surface area
- High thermal stability

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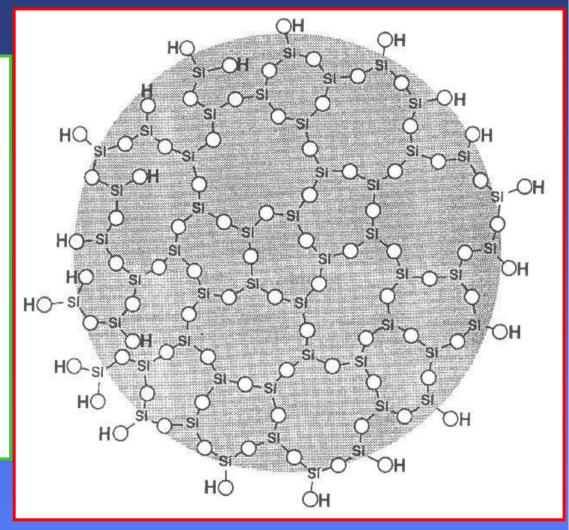
Insulator oxides

Silica

Schematic representation of a dehydrated but fully hydroxylated **colloidal silica particle**. The 4th oxygen coordinated with Si is above or below the plane. The Si-O-Si bond angle may vary, but the Si-O distances are constant. (H. Bergna, The Colloid Chemistry of

Low thermal stability
 Large specific surface area

Silica, ACS, 1994, p. 9.)



Zeolites

Aluminosilicates

Zeolite frameworks buit up from sodalite units:

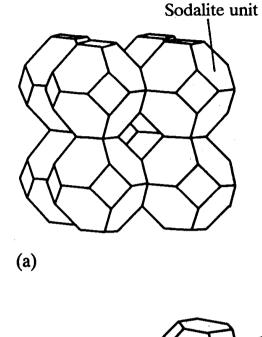
(a) sodalite,

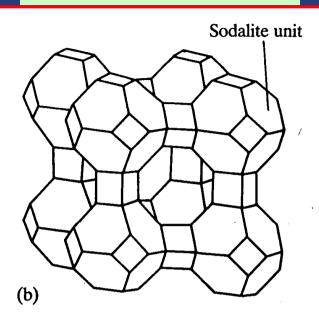
(b) A-zeolite,

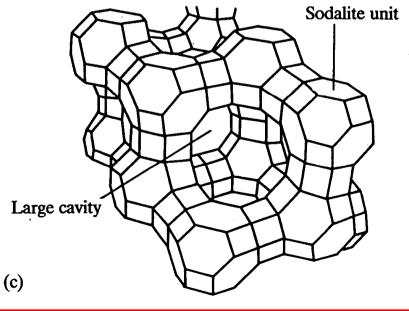
(c) faujasite (X- and Y-zeolite).

(L. Smart, E. Moore, 'Solid State Chemistry', Chapman et Hall, 1992)

Low thermal stability
Very large surface area







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→ Impregnation of the support with the precursor of the active phase.

Support: high surface area oxide (100 - 400 m².g⁻¹), high internal porosity (1 mL.g⁻¹). **Precursor**: soluble in the solvent and firmly bonded on the surface after the impregnation. **Active phase**: obtained after transformation of the precursor (activation of the catalyst).

Ex.: Shell 405 catalyst for N₂H₄ decomposition:

Support: gamma alumina, specific surface area: 100-200 m².g⁻¹.

Precursor: hexachloroiridic acid H_2IrCl_6 in aqueous solution.

Impregnation procedure: wetness impregnation procedure. The volume of the impregnating solution corresponds to the volume of the porosity.

Drying: fixation of the precursor on the hydroxyl groups present at the alumina surface.

Activation, reduction in H₂, formation of iridium crystallites onto the surface of alumina.

The procedure is repeated in order to obtain the expected load on the alumina surface.

What is a solid catalyst ?Preparation of metal supported catalysts

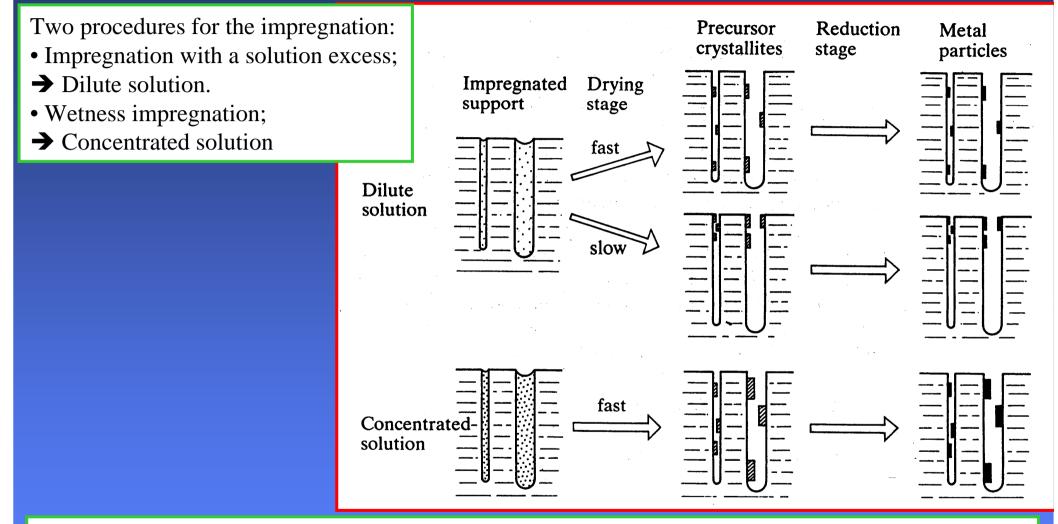
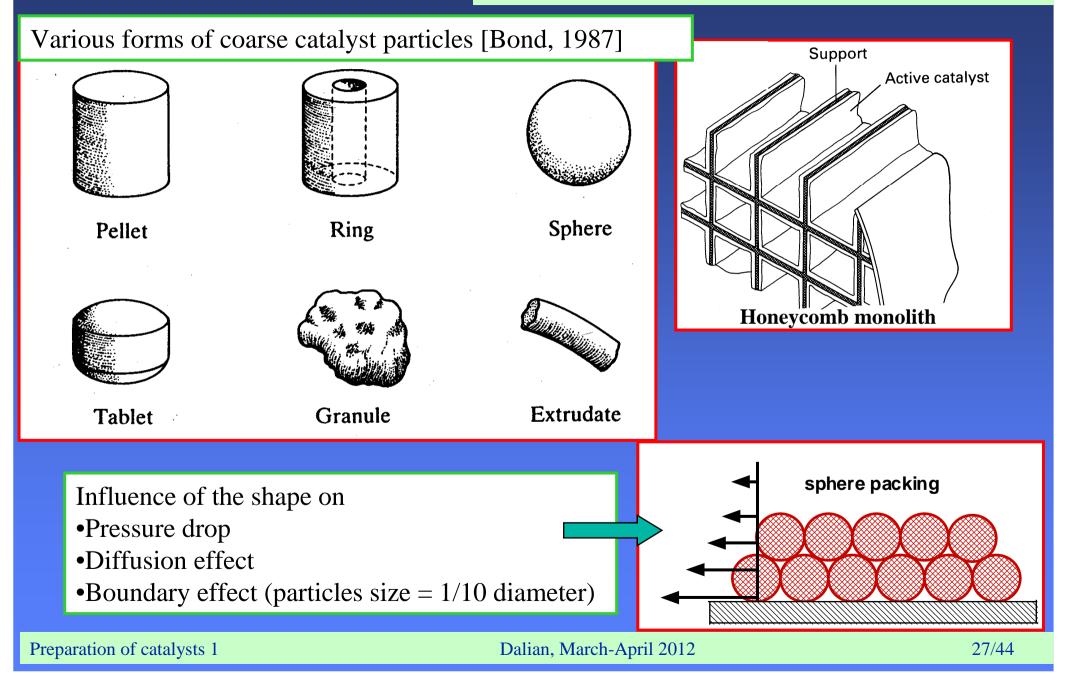


Illustration of the stages in the preparation of supported metal catalysts: the pores of the support are initially impregnated with either a dilute or a concentrated solution of the metal precursor [88-B].

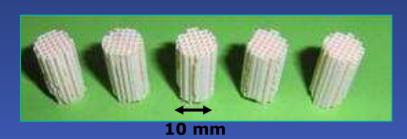
Preparation of catalysts 1

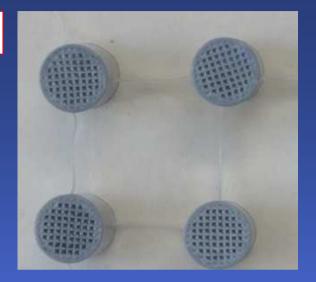
Forms and shapes of catalysts



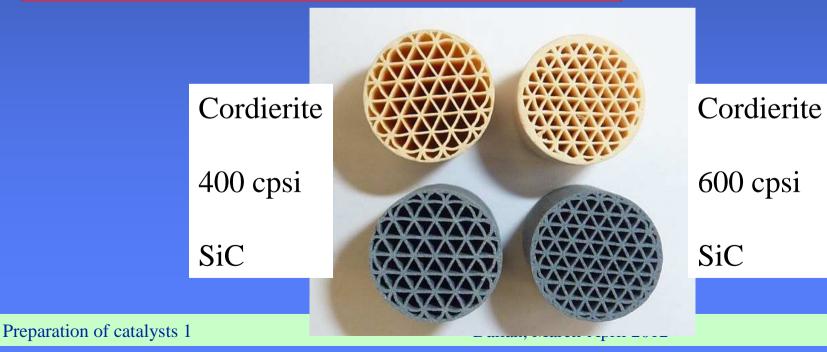
Cellular ceramics

1) Small honeycomb monoliths: square channels





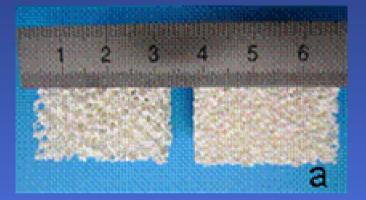
2) Small honeycomb monoliths: triangular channels



Cellular ceramics

3) Foams: interconnected pores

block of foam (alumina)

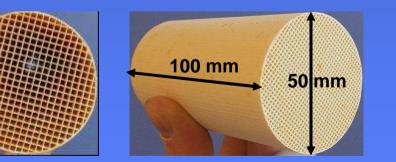


cylindrical-shaped foam (mullite).



4) Large honeycomb monoliths

Monolith before preparation 100 or 400 cpsi Cordierite or mullite





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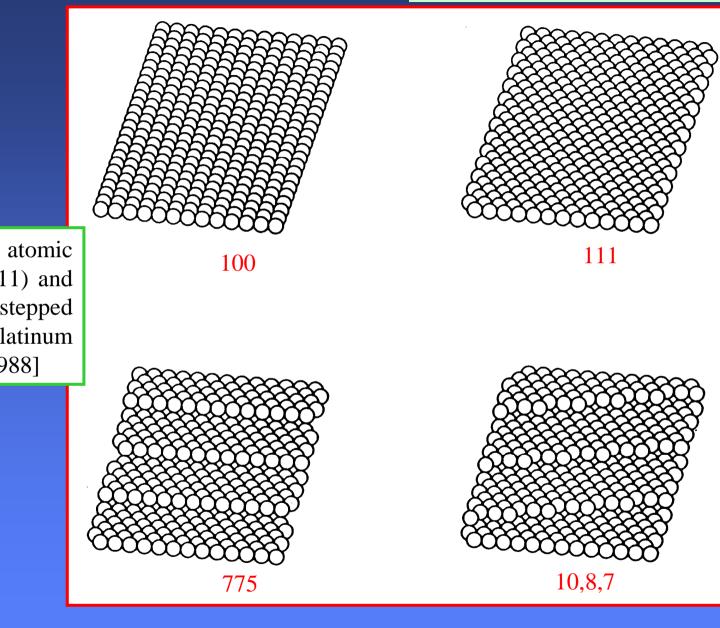
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Different tools are necessary to characterize the catalysts and their surfaces

Technique	Property probed
	Bulk information:
Elemental analysis	chemical composition:
Powder X-ray diffraction	phase composition, average crystallite size
Electron microscopy	texture, porosity, crystallite size distribution
EXAFS	environment of the target atoms
Infrared and Raman spectroscopy	structure
	Surface information
Physisorption	total surface area, pore volume,
	pore size distribution
Chemisorption	active surface area, dispersion
Work function	direction of flow of electrons to or from the
	surface
XPS	surface composition, oxidation states
Probe molecules (NH ₃ , CO,)	acidity, basicity, metal surfaces
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Ideal surfaces



Ball model of idealized atomic structures of the **platinum** (111) and (100) crystal faces, the stepped platinum (775) and kinked platinum (10,8,7) surfaces [Campbell, 1988]

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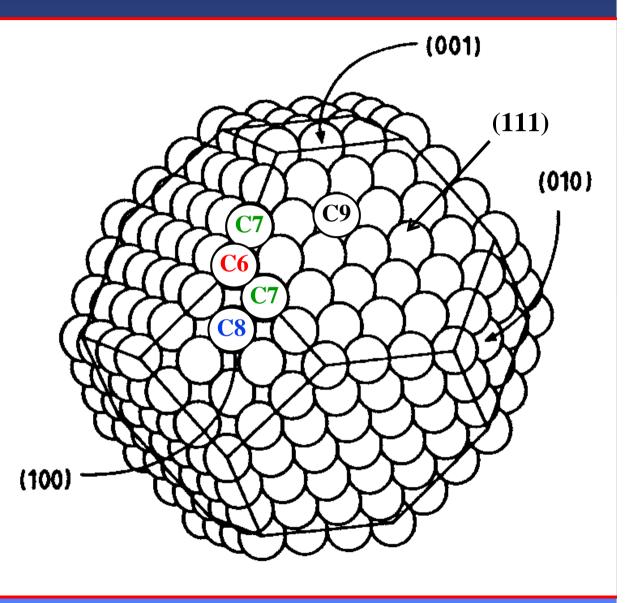
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Ideal three-dimensional model

Close packed cubic arrangement. Truncated octahedron with faces (100) and (111) [Thomas & Thomas, 1997]

Neighbour number

C6 (corner)	6
C7 (edge)	7
C8 (square surface)	8
C9 (hexagonal surface)	9
Bulk	12

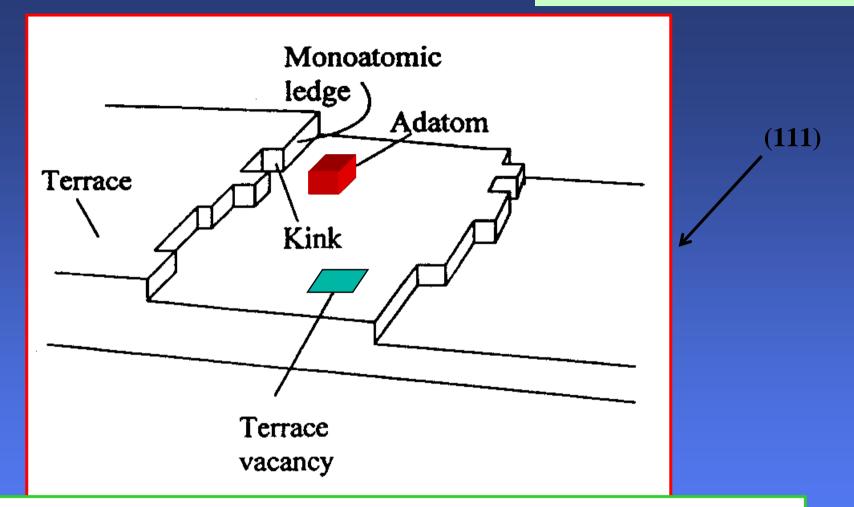


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Real surfaces

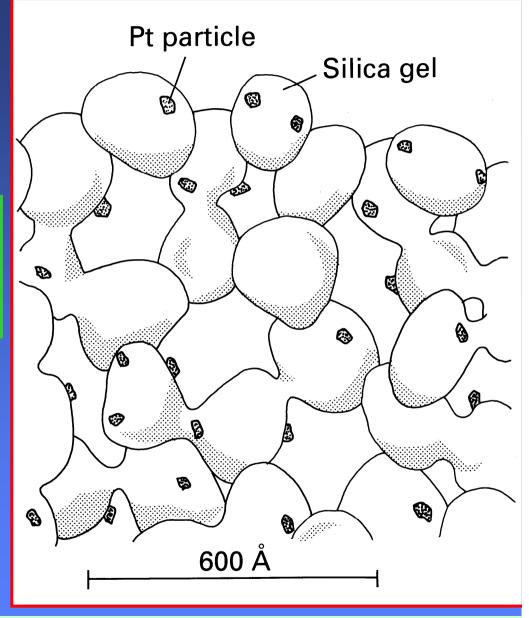


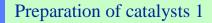
Model of a heterogeneous solid surface depicting different surface sites. These sites (step, kink, terrace, adatom and vacancy) are distinguishable by their number of nearest neighbors [Attard & Barnes, 1998].

Model of supported catalysts

Schematic diagram of **platinum particle** supported on silica gel Pt/SiO_2

We have the same model for Ir/Al_2O_3 .



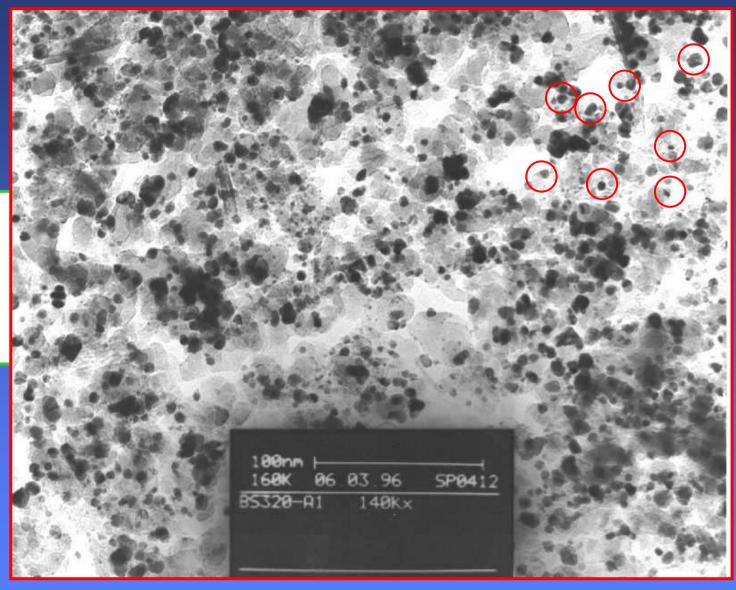


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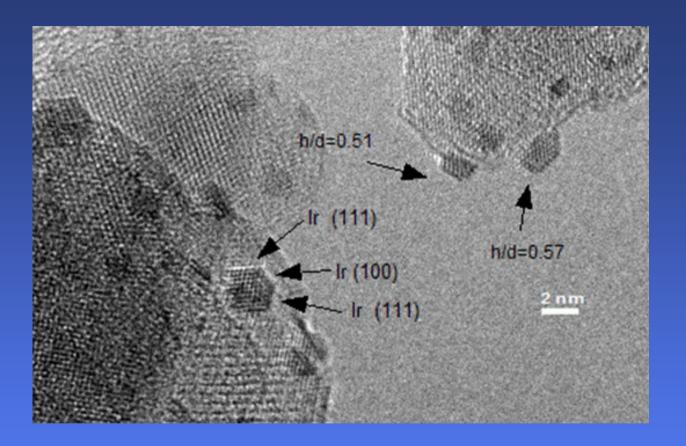
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Real surfaces probed by electron microscopy

Transmission electron micrograph of an Ir/Al₂O₃ catalyst. the bar indicates the scale 100 nm.



Real surfaces probed by electron microscopy



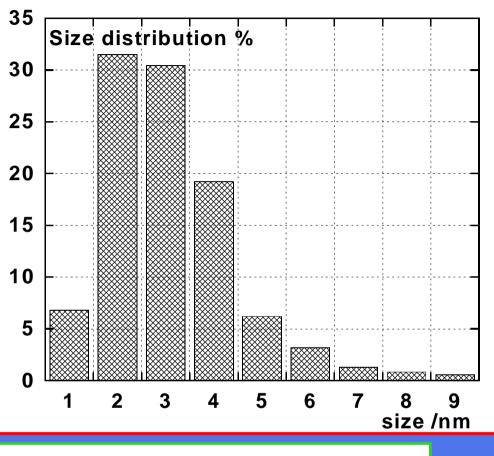
TEM picture of Ir/Al2O3 sample showing the hemi-cuboctahedral shape of iridium crystallites.

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Particle size distribution

Particle size distribution of a Ir/Al_2O_3 catalyst. The data are from the previous micrograph (manual counting).



	Different mean sizes (values in nm):	calculated	experimental	
	Number $\Sigma x_i d_i$ (x_i = number fraction)	3.1		
	Surface $\sum x_i d_i^3 / \sum x_i d_i^2$	4.7	4.7 (dispersion)	
	Volume $\Sigma x_i d_i^4 / \Sigma x_i d_i^3$	5.6	5.5 (XRD)	
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The active centers

Activity:	specific activity (per g of catalyst) intrinsic activity (per active center) transformation rate: %-R _A = 100 x number of A-mol converted/ total number of A-mol
Selectivity:	choice between several paths $A \rightarrow B$ or $A \rightarrow C$ selectivity factor $S_B = x_B/(x_B + x_C)$ $x_B = $ mol-fraction of B depends on the activation energies selective poisoning
Stability:	thermal stability: sintering effect mechanical stability: attrition chemical stability: modification of the active sites poisons (sulfur, ammonia, carbon monoxide,)

Catalyst activity

→ Influence of dispersion or crystallite size on activity?

Example: decomposition of hydrazine

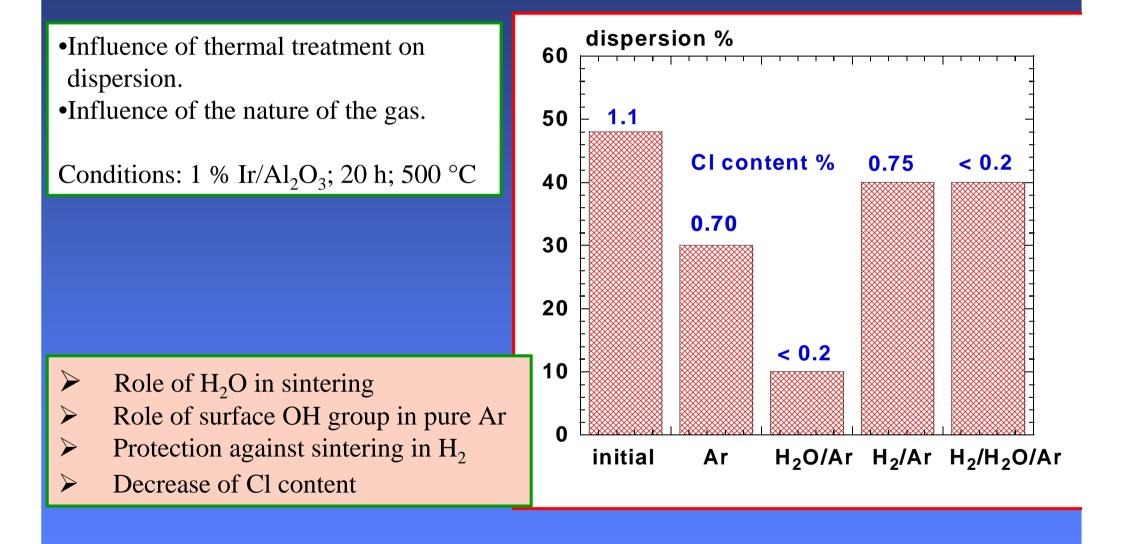
Two successive reactions:

$3 N_2 H_4$	→	$4 \text{ NH}_3 + \text{N}_2$	(1)
4 NH ₃	→	$2 N_2 + 6 H_2$	(2)

Study of step 1: decomposition of hydrazine into ammonia

Catalysts: 1 %-Ir/Al ₂ O ₃ diluted in alumina (1 to 20)						
catalyst	dispersion	activity	intrinsic activity			
	in %	mol/g.h	(mol-N ₂ H ₄)/(mol-Ir).h			
А	48	2.2	88400			
В	10	0.50	96000			
С	3	0.13	95000			
D	40	1.9	95000			
Different specific activities						
Same intrinsic activity						
No influence of crystallite size						

Catalyst stability



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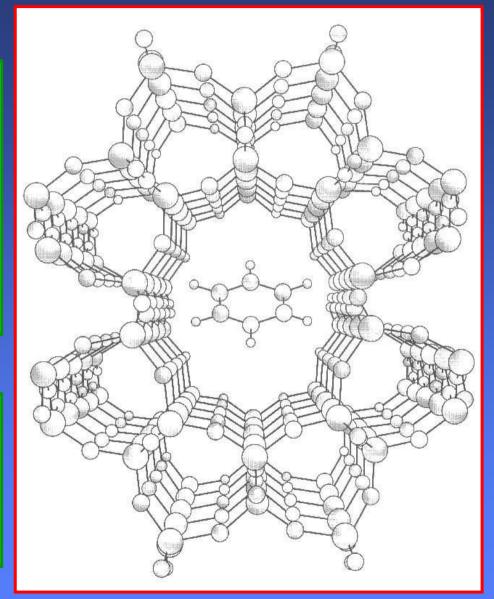
Catalyst selectivity

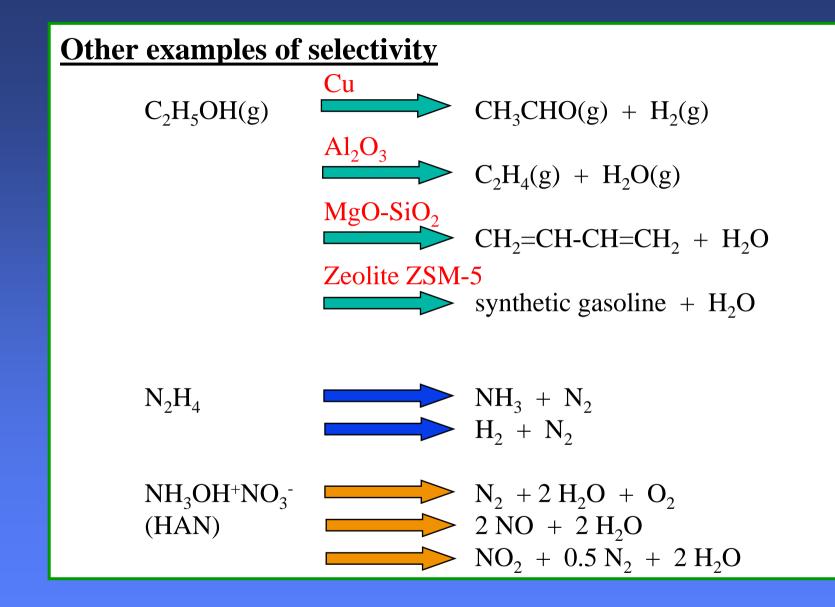
Shape selectivity in zeolites

A view through the channels of theta-1 zeolite with an adsorbed benzene molecule in one of the channels [Shriver, Atkins, 1994] Opening of the channels typically 3 to 10 Å for different zeolites.

→ Microporous materials

- ➔ Absorption of molecules small enough to enter the channels.
- \rightarrow Exclusion of larger molecules.
- → Control over catalytic reactions unattainable with silica or alumina.





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